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## NOTIFICATION OF ELECTION

(PCT Rule 61.2)

From the INTERNATIONAL BUREAU

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<b>Date of mailing (day/month/year)</b> 14 June 2000 (14.06.00)	
<b>International application No.</b> PCT/NO99/00293	<b>Applicant's or agent's file reference</b> 101295G
<b>International filing date (day/month/year)</b> 21 September 1999 (21.09.99)	<b>Priority date (day/month/year)</b> 27 October 1998 (27.10.98)
<b>Applicant</b> LUND, Are et al	

1. The designated Office is hereby notified of its election made:



in the demand filed with the International Preliminary Examining Authority on:

02 May 2000 (02.05.00)



in a notice effecting later election filed with the International Bureau on:

2. The election ☒ was

was not

made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

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REC'D 18 JUL 2000

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## INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant's or agent's file reference 101295G	<b>FOR FURTHER ACTION</b>	See Notification of Transmittal of International Preliminary Examination Report (Form PCT/IPEA/416)
International application No. PCT/NO99/00293	International filing date (day/month/year) 21/09/1999	Priority date (day/month/year) 27/10/1998
International Patent Classification (IPC) or national classification and IPC F17D3/14		
Applicant LEIV EIRIKSSON NYFOTEK AS et al.		

1. This international preliminary examination report has been prepared by this International Preliminary Examining Authority and is transmitted to the applicant according to Article 36.


2. This REPORT consists of a total of 4 sheets, including this cover sheet.

- ☐ This report is also accompanied by ANNEXES, i.e. sheets of the description, claims and/or drawings which have been amended and are the basis for this report and/or sheets containing rectifications made before this Authority (see Rule 70.16 and Section 607 of the Administrative Instructions under the PCT).

These annexes consist of a total of sheets.

3. This report contains indications relating to the following items:

- I ☒ Basis of the report
- II ☐ Priority
- III ☐ Non-establishment of opinion with regard to novelty, inventive step and industrial applicability
- IV ☐ Lack of unity of invention
- V ☒ Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement
- VI ☐ Certain documents cited
- VII ☐ Certain defects in the international application
- VIII ☐ Certain observations on the international application

Date of submission of the demand  02/05/2000	Date of completion of this report  14.07.2000
Name and mailing address of the international preliminary examining authority:  European Patent Office D-80298 Munich Tel. +49 89 2399 - 0 Tx: 523656 epmu d Fax: +49 89 2399 - 4465	Authorized officer  Schibli, T  Telephone No. +49 89 2399 2937



**INTERNATIONAL PRELIMINARY  
EXAMINATION REPORT**

International application No. PCT/NO99/00293

**I. Basis of the report**

1. This report has been drawn on the basis of (*substitute sheets which have been furnished to the receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed to the report since they do not contain amendments.*):

**Description, pages:**

1-11 as published

**Claims, No.:**

1-18 as published

**Drawings, sheets:**

1/2,2/2 as published

2. The amendments have resulted in the cancellation of:

- ☐ the description, pages:  
☐ the claims, Nos.:  
☐ the drawings, sheets:

3. ☐ This report has been established as if (some of) the amendments had not been made, since they have been considered to go beyond the disclosure as filed (Rule 70.2(c)):

4. Additional observations, if necessary:

**INTERNATIONAL PRELIMINARY  
EXAMINATION REPORT**

International application No. PCT/NO99/00293

**V. Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement**

**1. Statement**

Novelty (N)	Yes: Claims 1-18
	No: Claims
Inventive step (IS)	Yes: Claims 1-18
	No: Claims
Industrial applicability (IA)	Yes: Claims 1-18
	No: Claims

**2. Citations and explanations**

**see separate sheet**

**INTERNATIONAL PRELIMINARY  
EXAMINATION REPORT - SEPARATE SHEET**

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International application No. PCT/NO99/00293

The problem underlying the present invention is the risks which appear when water contained in hydrocarbons freezes occasionally to form gas hydrates together with components of the hydrocarbon fluid. Hazardous clogging of pipelines may occur.

The Search Report comprises 2 documents. In both, water is separated and has to be removed in an additional piping system.

The invention according to claim 1 reverses this notion by freezing all water to form gas hydrate particles, making use of a reactor into which already frozen gas hydrate particles are recirculated. It has been experimented by the inventors that the already frozen particles are easily transportable with the liquid flow without causing the above-mentioned problems.

In claim 12 the means are stated which perform the method of claim 1.

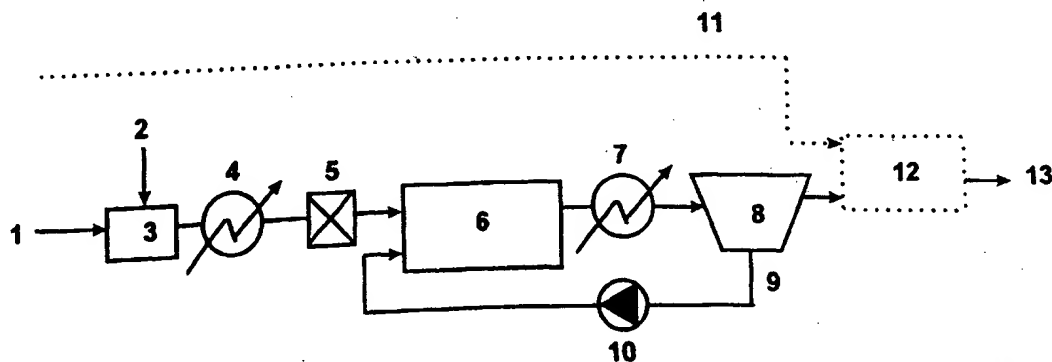
These means are clearly different from those shown in the prior art which provide for a separation of the water containing component or the water respectively.



## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<b>(51) International Patent Classification <sup>7</sup> :</b> <b>F17D 3/14, C10G 33/06</b>	<b>A1</b>	<b>(11) International Publication Number:</b> <b>WO 00/25062</b> <b>(43) International Publication Date:</b> 4 May 2000 (04.05.00)
<b>(21) International Application Number:</b> PCT/NO99/00293 <b>(22) International Filing Date:</b> 21 September 1999 (21.09.99) <b>(30) Priority Data:</b> 19985001      27 October 1998 (27.10.98)      NO <b>(71) Applicant (for all designated States except US):</b> LEIV EIRIKSSON NYFOTEK AS [NO/NO]; P.O. Box 62, Pirsenteret, N-7005 Trondheim (NO). <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only):</b> LUND, Are [NO/NO]; Sildråpeveien 23D, N-7048 Trondheim (NO). LYSNE, David [NO/NO]; Mikkel Mærks vei 1, N-7020 Trondheim (NO). LARSEN, Roar [NO/NO]; Humlehaugveien 1, N-7054 Ranheim (NO). HJARBO, Kai, W. [NO/NO]; Markaplassen 113, N-7054 Ranheim (NO). <b>(74) Agent:</b> BRYN & AARFLOT AS; P.O. Box 449 Sentrum, N-0104 Oslo (NO).		<b>(81) Designated States:</b> AE, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).  <b>Published</b> <i>With international search report.</i>

**(54) Title:** METHOD AND SYSTEM FOR TRANSPORTING A FLOW OF FLUID HYDROCARBONS CONTAINING WATER

**(57) Abstract**

Method for transporting a flow of fluid hydrocarbons containing water through a treatment and transportation system including a pipeline, wherein the flow of fluid hydrocarbons is introduced into a reactor where it is mixed with particles of gas hydrates which are also introduced into said reactor, the effluent flow of hydrocarbons from the reactor is cooled in a heat exchanger to ensure that all water present therein is in the form of gas hydrates, said flow is then treated in a separator to be separated into a first flow and a second flow, said first flow having a content of gas hydrate is recycled to the reactor to provide the particles of gas hydrates mentioned above, and said second flow is conveyed to a pipeline to be transported to its destination. System for treatment and transportation of a flow of fluid hydrocarbons containing water, which includes the following elements listed in the flow direction and connected with each other: connection to a hydrocarbon source (1), a first heat exchanger (4), a reactor (6), a second heat exchanger (7), a separator (8), and a pipeline (13); and in addition a line (9) which leads from the separator (8) to the reactor (6) and is provided with a pump (10) adapted to recycle material from the separator (8) back to the reactor (6).

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"Method and system for transporting a flow of fluid hydrocarbons containing water."

The present invention relates to a method and a system for transporting a flow of fluid (i.e. liquid or gaseous) hydrocarbons containing water. In the method said flow is transported through a treatment and transportation system including a pipeline.

The search for new oil or gas resources has now reached a stage where it is moving away from relatively easily accessible continental waters, and towards deeper waters. This trend is currently most visible in the Gulf of Mexico, but also offshore Norway, any large oil or gas discoveries in the future are primarily expected in deep waters ( $\geq 4-500$  m). This development gives rise to several technological challenges. However, solutions based on sub-sea installations and long distance transport to already existing production and processing facilities have already been in use for some time in the North Sea, especially in connection with economically marginal fields in the vicinity of older platforms. This technology will become steadily more prevalent in new field developments for deep water, but also in the increasing number of smaller projects in already developed areas.

Traditionally, in the North Sea, use of sub-sea templates and pipeline transport of the well-stream in multiphase pipelines has been restricted to a few tens of kilometers. However, better simulation and design tools, better equipment for partial separation, as well as pumping and boosting, has now led to solutions of this kind being used with transfer distances of up to 110 km in the Gulf of Mexico.

The single most challenging problem for these future trends in oil and gas exploration, is the presence of natural gas hydrates in transport pipelines and equipment. Natural gas hydrate is an ice-like compound consisting of light hydrocarbon molecules encapsulated in an otherwise unstable water crystal structure. These hydrates form at high pressures and low temperatures wherever a suitable gas and free water are present. These crystals can deposit on pipeline walls and in equipment, and in the worst case lead to complete plugging of the system. Costly and time-consuming procedures may be needed to restore flow



again. In addition to the mere economic consequences, there are also numerous hazards connected to hydrate formation and removal, and there are known instances of pipeline ruptures and loss of human lives due to gas hydrates in pipelines. Although hydrate is generally thought of as a problem mostly for gas production, there is now ample evidence that it is also a significant problem for condensate and oil production systems.

There are several available methods for dealing with hydrate problems. So far, the usual philosophy has been to take steps to avoid any hydrate formation at all. This can be achieved by keeping pressures low (often not possible from flow considerations), keeping temperatures high (usually by insulating - which does not protect against shutdowns or long distances), removing the water completely (costly equipment and difficult), or by adding chemicals that suppress hydrate formation thermodynamically. Insulation is very often used, but is not sufficient alone. Chemical addition, specifically methanol (MeOH) or ethylene glycol (EG), is therefore the most widespread hydrate control mechanism in the industry today. These antifreezes expand the pressure-temperature-area of safe operation, but are needed in large quantities - 50% of the total liquid fraction is not unusual in water-rich production. The use of MeOH in the North Sea may approach 3 kg per 1000 Sm<sup>3</sup> of gas extracted. The need for such large amounts places severe demands on logistics of transportation, storage and injection in offshore facilities with a deficiency of space. The transport and injection processes for MeOH in particular, are also plagued with numerous leakages and spills.

Inhibitor chemicals of different types are not only used in the pipeline transport and processing areas, but also extensively in drilling operations and wells.

Partly due to the huge amounts and large costs involved in using traditional inhibitors like MeOH, there has over the last decade been extensive efforts devoted to finding chemicals which may be effective at controlling hydrates at much lower concentrations.

Many oil companies and research institutes have contributed to this effort, and at present, the results are divided into three main categories: kinetic inhibitors, dispersants, and modifiers. Kinetic inhibitors have an affinity for the crystal

surface, and thereby can be used to prevent hydrate crystal growth. Dispersants act as emulsifiers, dispersing water as small droplets in the hydrocarbon liquid phase. This limits the possibilities for hydrate particles to grow large or to accumulate. The modifiers are to a certain extent a combination of the two other methods, attaching to the crystal surface, but also functioning as a dispersant in the liquid hydrocarbon phase. These methods have been somewhat successful, although there are practical drawbacks to most of them. The most significant problem, however, seems to be that all the best chemical additives thus far produced have significant negative environmental effects, and that no solution to this problem seems imminent - at least in the open literature.

There is growing understanding in the oil and gas industry that hydrate particles in a flow situation are not necessarily a problem per se. If the particles do not deposit on walls or equipment, and do not have a large impact on flow characteristics (i.e. their concentration is not too large), they simply flow with the rest of the fluids, without creating a problem situation. The challenge will therefore be to achieve this situation in a controlled manner, and making sure that hydrate formation does not take place randomly throughout the flow system.

Another aspect which will definitely be affected by the present invention, is corrosion in sub-sea pipelines. Huge sums of money and large resources in material and time are involved in protecting pipelines from corrosion, e.g. through conservative design (pipeline wall thickness, steel quality) and through the use of corrosion inhibitors. Not necessarily used in the same amounts per pipeline as the hydrate inhibitors, the total amounts of chemicals (sometimes with environmentally highly adverse effects) are huge, as they are used in such a great number of pipelines. Much of this corrosion is connected with free water, and successful results of the present invention may reduce this problem significantly.

The present invention provides a method for transporting a flow of fluid hydrocarbons containing water through a treatment and transportation system including a pipeline. According to the invention the flow of fluid hydrocarbons is introduced into a reactor where it is mixed with particles of gas hydrates which are also introduced into said reactor, the effluent flow of hydrocarbons from the reactor is cooled in a heat exchanger to ensure that all water present therein is in

the form of gas hydrates, said flow is then treated in a separator to be separated into a first flow and a second flow, said first flow having a content of gas hydrates is recycled to the reactor to provide the particles of gas hydrates mentioned above, and said second flow is conveyed to a pipeline to be transported to its destination.

Said flow of fluid hydrocarbons will normally come from a drilling hole well and will be relatively warm and will be under pressure. It is generally preferred to cool the flow of fluid hydrocarbons in a first heat exchanger before introducing said flow into the above-mentioned reactor.

It is sometimes desirable to add certain chemicals to the flow upstream to the reactor.

Before the flow enters the reactor it may advantageously be subjected to a mixing operation in order to disperse the water present as droplets in the fluid hydrocarbon phase.

The second flow from the separator may be mixed with wet gas in a mixing vessel before the flow is conveyed to the pipeline for further transport.

The method is particularly applicable in those cases where transportation takes place at a relatively low temperature, both on land in a cool climate and at the sea bottom.

When the surroundings are rather cool, one or more of the heat exchangers used may be an uninsulated pipe. When the surrounding temperature is sufficiently low, this will provide satisfactory cooling without any further cooling medium.

The invention also provides a system for treatment and transportation of a flow of fluid hydrocarbons containing water. The system includes the following elements listed in the flow direction and connected with each other so that the hydrocarbons may pass through the entire system (the numerals in parenthesis refer to the enclosed drawings which serve as illustration only):

connection to a hydrocarbon source (1),

a first heat exchanger (4),

a reactor (6),

a second heat exchanger (7),

a separator (8), and  
a pipeline (13);

and in addition a line (9) which leads from said separator (8) to the reactor (6) and is provided with a pump (10) adapted to recycle material from the separator (8)  
5 back to the reactor (6). The pump may be any kind of pump, but it may advantageously be of a type which crushes the hydrate particles into more and smaller particles with a larger total crystal surface.

The inside of the system, in particular the inside of the reactor may be coated with a water repellent material. Tubing may also advantageously be  
10 provided with such a coating material.

The system preferably includes a mixer or a choke (5) upstream to the reactor (6).

In many cases it is advantageous to add different chemicals to the flow of hydrocarbons, in particular during start-up and when changes are made in the  
15 operation. The system accordingly contains for such purpose means for adding chemicals to the flow.

In the following the present method and system will be described in more detail, again with reference to the drawings.

In a first embodiment (fig. 1) warm oil/condensate/hydrate-forming  
20 components and water under pressure (1) are mixed with any desired chemicals (2) in a mixing means (3). If much water is initially present, some of the water is preferably separated off before mixing said components and water with chemicals. The chemicals in question may be nucleating agents for hydrate, emulsion-  
breakers/-formers, wax inhibitors or any type of chemical used for  
25 transportation/storage of said fluid. The chemicals used should be acceptable for the environment and should generally be used during start-up only. In any case the consumption of chemicals will be much lower during continuous operation than previous transportation/storage systems, and chemicals may even be left out completely.

30 The fluid from the mixer (3) may be cooled to a temperature just above the hydrate equilibrium curve of the fluid (the melting curve of hydrate) in a heat

exchanger (4). At the bottom of the ocean said heat exchanger may be an uninsulated tube, or it may be any type of cooler.

The fluid from the heat exchanger (4) is conveyed to a mixer (5) which may be any type of mixer. The mixer distributes the water in the fluid hydrocarbons as droplets. It should be noted that the mixer is not strictly necessary. The question whether or not a mixing operation is necessary depends on the characteristics of the fluid, i.e. the ability of the fluid to distribute the water as droplets in the fluid without any other influence than the turbulence which occurs when the fluid flows through a pipe.

The fluid from the mixer (5) is conveyed into a reactor (6), where it is mixed with cold (temperature below the melting temperature of the gas hydrate) fluid from a separator (8) (see below). Said cold fluid from the separator (8) contains small particles of dry hydrate.

The water which is present in the fluid from the mixer (5) will moisten dry hydrate from the separator (8) in the reactor (6). In the reactor (6) the water which moistens the dry hydrate will immediately be converted to hydrate. New hydrate which is formed will accordingly increase the size of the hydrate particles from the separator (8) and also form new small hydrate particles when larger hydrate particles break up. New hydrate seed may also be formed elsewhere in the reactor (6).

Sub-cooling (the actual temperature being lower than the hydrate equilibrium temperature) of the fluid is required to form hydrates. The necessary extent of sub-cooling for formation of hydrate in the reactor (6) is accomplished by adding sufficient cold fluid from the separator (8). Cooling may also come from the reactor walls of the reactor (6) or from separate cooling ribs in said reactor. Undesired fouling or formation of deposits in the reactor (6) may be avoided by coating all surfaces with a water-repellent coating.

From the reactor (6) the fluid is cooled down in a second heat exchanger (7). At the bottom of the ocean said cooler may be an uninsulated pipe. The heat exchanger (7) may also be any type of cooler which even may be integrated as a part of the reactor (6).

In the separator (8) some of the total amount of hydrate particles and excess fluid are separated from the rest and conveyed out to a pipeline (13) or first through a mixing means (12) to be mixed with wet gas (11) before entering the pipeline (13).

5        Residual amounts of the total amount of hydrate particles and residual fluid from the separator (8) are recycled through a line (9) by means of a pump (10) back to the reactor (6). The separator (8) may be any type of separator. Similarly, the pump (10) may be any type of pump, but it is important that it can handle the hydrate particles. It may advantageously be of a type which crushes the hydrate  
10       particles into more and smaller particles with a larger total crystal surface. A further cooler may be included in the line (9) either before or behind the pump (10).

      Wet gas (11) under pressure may be mixed with the flow of fluid from the separator (8) in a mixing means (12). Free water in the wet gas is absorbed by  
15       the dry hydrate from the separator (8) in the mixing means (12). In the mixing means (12) the water which moistens the dry hydrate will readily be converted to hydrate. The new hydrate formed will then increase the size of the hydrate particles from the separator (8) and may also form new small hydrate particles when larger hydrate particles are broken apart. New hydrate seed may also be  
20       formed elsewhere in the mixing means (12). At the outlet of the mixing means (12) connected to the pipeline (13) all free water has been converted to hydrate.

      At the beginning of the pipeline, either sub-sea at a wellhead template, or onboard a minimum processing platform, water separation is expected to be efficient enough so that after cooling and condensation, no more than 5-10 vol%  
25       water is present in the fluid stream.

      After this separation stage, the fluids are cooled rapidly towards hydrate stability temperatures in exposed (uninsulated) pipes of the necessary length. The phases are also mixed, to provide a large interfacial surface area. Minute amounts of chemicals may be needed at this stage, e.g. in connection with a start-  
30       up situation. A mixer will disperse the water as droplets. Upon next entering the hydrate reactor part of the system, hydrate particles and a cold fluid stream are mixed in from a downstream separator. Water wetting of the hydrate particles will

take place, and hydrate growth will therefore mainly be from existing particles and outwards. The hydrate formation process is thus aided by the addition of cold fluid (inside the stable hydrate pressure-temperature region), and - most important - the already present hydrate particles. Further cooling takes place through the reactor.

5 According to a second embodiment (see fig. 2) the fluid hydrocarbon is preferably a wet hydrocarbon gas. The method of this embodiment is particularly applicable at the sea bottom.

To a great extent the discussion of the first embodiment above will also apply to this second embodiment. In the following, particularly those features  
10 which are more or less different will be discussed.

Warm hydrocarbon gas (1) under pressure is mixed with any desired chemicals (2) in a mixing means (3). Chemicals may also be added to the system in the reactor (6).

The flow from the mixer (3) may be cooled to a temperature just above the  
15 hydrate equilibrium curve of the flow (the melting curve of hydrate) in a heat exchanger (4) and/or through a choke (5) which may be a part of the reactor (6). At the bottom of the ocean said heat exchanger may be an uninsulated tube, or it may be any type of cooler.

The flow from the choke (5) is conveyed into the reactor (6), where it is  
20 mixed with cold (temperature below the melting temperature of the gas hydrate) fluid from a second separator (8) (see below). Said cold fluid from the separator (8) contains small particles of dry hydrates.

Free water and water condensing from hydrocarbon gas in the flow from the choke (5) will moisten dry hydrate from the separator (8) in the reactor (6). In  
25 the reactor (6) the water which moistens the dry hydrate will immediately be converted to hydrate. New hydrate which is formed will accordingly increase the size of the hydrate particles from the separator (8) and also form new small hydrate particles when larger hydrate particles break up. New hydrate seed may also be formed elsewhere in the reactor (6).

30 In a first separator (14) hydrocarbon gas is separated from the flow and conveyed out to a pipeline (15). The separator (14) may be any type of separator.

The rest of the flow is conveyed to the second separator (8) where some of the total amount of hydrate particles and excess fluid are separated from the rest and conveyed out to a pipeline (13).

Residual amounts of the total amount of hydrate particles and residual fluid  
5 from the separator (8) are recycled through a line (9) by means of a pump (10) back to the reactor (6). The separator (8) may be any type of separator. Similarly, the pump (10) may be any type of pump, but it is important that it can handle the hydrate particles.

Additional cooled condensate under pressure may be added (16) to said  
10 recycled flow in order to dilute the hydrate particle concentration and as a cooling media. The addition may be made at any point between heat exchanger (7) and reactor (6).

Hot hydrocarbon gas, either sub-sea at a wellhead template, or from a minimum processing platform, is expected to be saturated with water vapour at  
15 the beginning of the pipeline.

After the wellhead template or platform, the flow is cooled rapidly towards hydrate stability temperature in exposed (uninsulated) pipes of the necessary length or through a choke. Minute amounts of chemicals may be needed at this stage, e.g. in connection with a start-up situation. Upon entering the hydrate  
20 reactor part of the system, hydrate particles and cold fluid stream, are mixed in from a downstream separator. Water vapour from the hydrocarbon gas phase will condensate and water wetting of the hydrate particles will take place. From this stage hydrate growth will therefore mainly take place from existing particles. The hydrate formation process is thus aided by the addition of cold fluid (inside the  
25 stable hydrate pressure-temperature region), and-most important – the already present hydrate particles. Further cooling takes place through the reactor. Hydrocarbon fluid condensed from the cooled hydrocarbon gas will add to the fluid in the reactor.

A further, general discussion of the present invention is given in the  
30 following.



Free water in the pipeline proper will tend to act as a "bonding agent" between hydrate and pipe walls. The inner surface of the hydrate reactor can be treated to become non-wetting with respect to water.

All of the water in the stream will be converted to dry hydrate particles by the time it reaches the end of the hydrate reactor. Before the stream reaches the downstream separator it is cooled close to ambient temperature in exposed (uninsulated) pipes of necessary length. In the separator some of the cold hydrocarbon fluids and dry hydrate particles are taken out, and re-injected at the reactor inlet, as described above.

If injection of wet gas (from the initial separation stage) is desirable, it may take place after the separation/recirculation point (8), into the stream with fully converted hydrates. These fluids may then flow through a similar hydrate reactor to achieve full conversion before the main pipeline. However, no separation and recirculation is viewed as necessary for this stage.

The main pipeline starts immediately after the separator or the wet gas hydrate reactor.

With the water being in hydrate form, and the hydrate particles being dry (no excess water) it has been known experimentally in flow loops with both model systems and with real field fluids and pressures and temperatures, that the resulting hydrate powder is easily transportable with the liquid flow. These tests also indicated that the particles will not aggregate or deposit on pipe walls or equipment - not even in the case of longtime shut-downs. This particular phenomenon has been studied by the inventors for several years. It is also a great advantage of the present invention that the absence of free water will reduce the risk of corrosion in pipelines and other installations.

The hydrate powder will not melt back to free the water and natural gas until temperatures rise or pressures become too low - which in reality will be at the end of the transport pipe, where the process will not be problematic. The powder can be mechanically separated from the bulk liquid phase by a sieve (unlike dispersant-induced emulsions which are often difficult to break). Another method would be to melt the hydrates in a separator where the residence time is long enough for the emerging water to separate out from the hydrocarbon liquids.

Depending on the fluid system, the particle density may even deviate enough from the bulk liquid so that the particles may easily be separated off.

The present invention is expected to create considerable positive environmental effects. The development of a safe and efficient way to transport free water in the form of hydrate particles will dramatically reduce the need for a host of different chemical additives which are used today, both hydrate and corrosion inhibitors. This will impact all aspects of the hydrocarbon production process, from working conditions on production and processing facilities, to the effect on the environment through leaks, accidental discharges or injection system malfunctioning.

A secondary, but no less important, environmental effect will be the improved safety aspects in pipeline operation: with the hydrate plugging and corrosion risks minimized, the danger of pipeline ruptures and large-scale blowouts will also be lowered. It should also be noted that a pipeline in thermal equilibrium with its surroundings will be safer with respect to melting of hydrates in the surrounding sediments which may induce instabilities (settling and landslides). This aspect is in addition to the fact that a cold fluid stream without temperature-induced changes in the fluid composition and properties makes the whole pipeline a more well-defined system to operate. This will not cause additional problems in itself, as pipeline transport over any significant distance will eventually reach ambient temperature also in traditional transport solutions.

The very limited use of chemicals according to the present invention also has the effect that the flow of fluid hydrocarbons is more suitable for its final use than known from the prior art. Thus, e.g. antifreeze such as methanol may have to be removed before the hydrocarbons are used in different processes, such as for polymerization purposes. Such removal is generally very costly.

PATENT CLAIMS

1. Method for transporting a flow of fluid hydrocarbons containing water through a treatment and transportation system including a pipeline, characterized  
5 in that the flow of fluid hydrocarbons is introduced into a reactor where it is mixed with particles of gas hydrates which are also introduced into said reactor, the effluent flow of hydrocarbons from the reactor is cooled in a heat exchanger to ensure that all water present therein is in the form of gas hydrates, said flow is then treated in a separator to be separated into a first flow and a second flow, said  
10 first flow having a content of gas hydrate is recycled to the reactor to provide the particles of gas hydrates mentioned above, and said second flow is conveyed to a pipeline to be transported to its destination.
2. The method of claim 1, characterized in that the flow of fluid hydrocarbons  
15 is cooled in a first heat exchanger before being introduced into the reactor.
3. The method of any of claims 1 and 2, characterized in that desired chemicals are added upstream to the reactor.
- 20 4. The method of any of claims 1-3, characterized in that the flow of fluid hydrocarbons is subjected to a mixing operating before introduction into the reactor to disperse the water present as droplets in the fluid hydrocarbon phase.
5. The method of any of claims 1-4, characterized in that said second flow  
25 from the separator is mixed with wet gas before it is conveyed to the pipeline.
6. The method of any of claims 1-5, characterized in that the method is performed at the sea bottom.
- 30 7. The method of any of claims 1-6, characterized by using an uninsulated pipe as heat exchanger when the surrounding temperature is sufficiently low.

8. The method of any claims 1-7, characterized in that the fluid hydrocarbons are hydrocarbon gas.

9. The method of any of claims 1-8, characterized in that the hydrocarbon flow is conveyed through a choke which is arranged upstream of the reactor or is a part of the reactor.

10. The method of any of claims 1-9, characterized in that the flow from the reactor conveyed through a first separator to be separated in a hydrocarbon gas flow and a flow which is subsequently subjected to separation in a second separator into said first and second flow.

11. The method of claim 10, characterized in that cooled condensate under pressure is added to said first flow which is recycled to the reactor.

12. System for treatment and transportation of a flow of fluid hydrocarbons containing water, characterized in that it includes the following elements listed in the flow direction and connected with each other:

connection to a hydrocarbon source (1),

a first heat exchanger (4),

a reactor (6),

a second heat exchanger (7),

a separator (8), and

a pipeline (13);

and in addition a line (9) which leads from the separator (8) to the reactor (6) and is provided with a pump (10) adapted to recycle material from the separator (8) back to the reactor (6).

13. The system of claim 12, characterized in that the inside of the reactor (6) is coated with a water-repellent material.

14. The system of any of claims 12 and 13, characterized in that it includes a mixer (5) between the first heat exchanger (4) and the reactor (6).

5 15. The system of any of claims 12-14, characterized in that it includes means (2) for adding chemicals to the flow.

16. The system of any of claims 12-15, characterized in that it includes means (12) between the separator and the pipeline for mixing the flow from the separator (8) with wet gas (11) before said flow enters the pipeline (13).

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17. The system of any of claims 12-16, characterized in that it includes a separator (14) between the second heat exchanger (7) and the separator (8) for recovering hydrocarbon gas from the flow.

15

18. The system of any of claims 12-17, characterized in that it comprises means (16) for adding cooled condensate under pressure to the line (9) from the separator (8) to the reactor (9).

Fig. 1

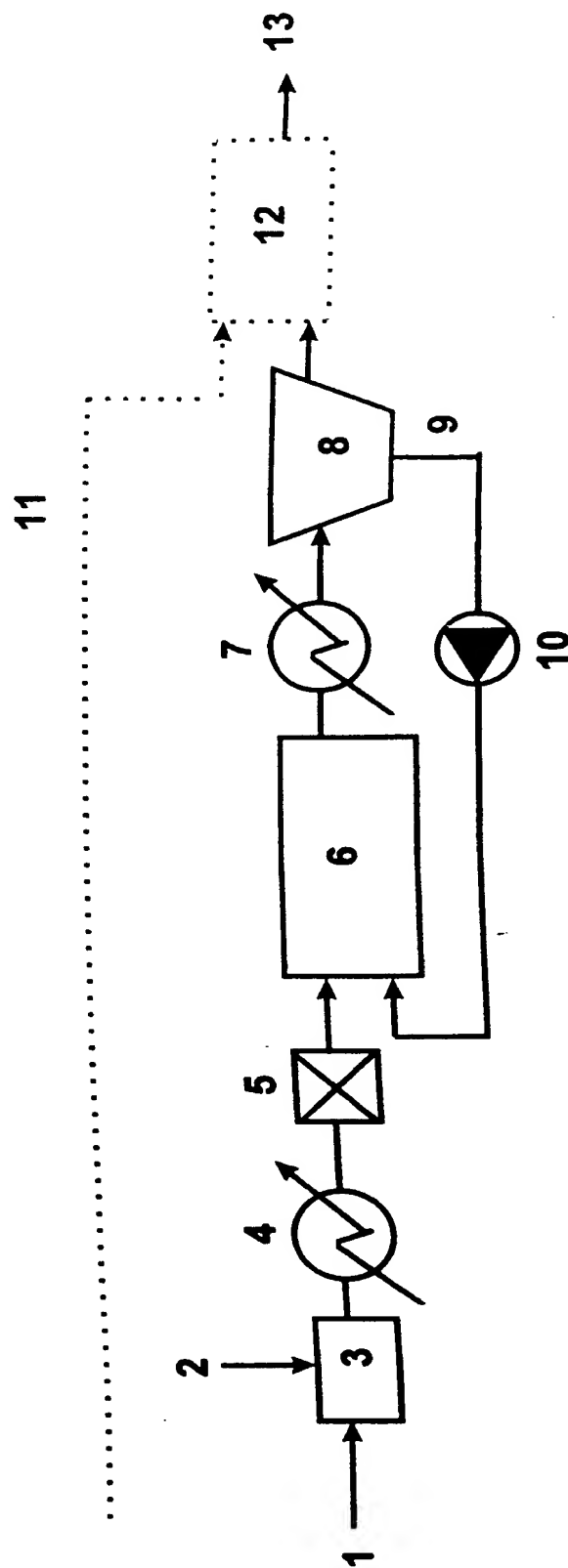
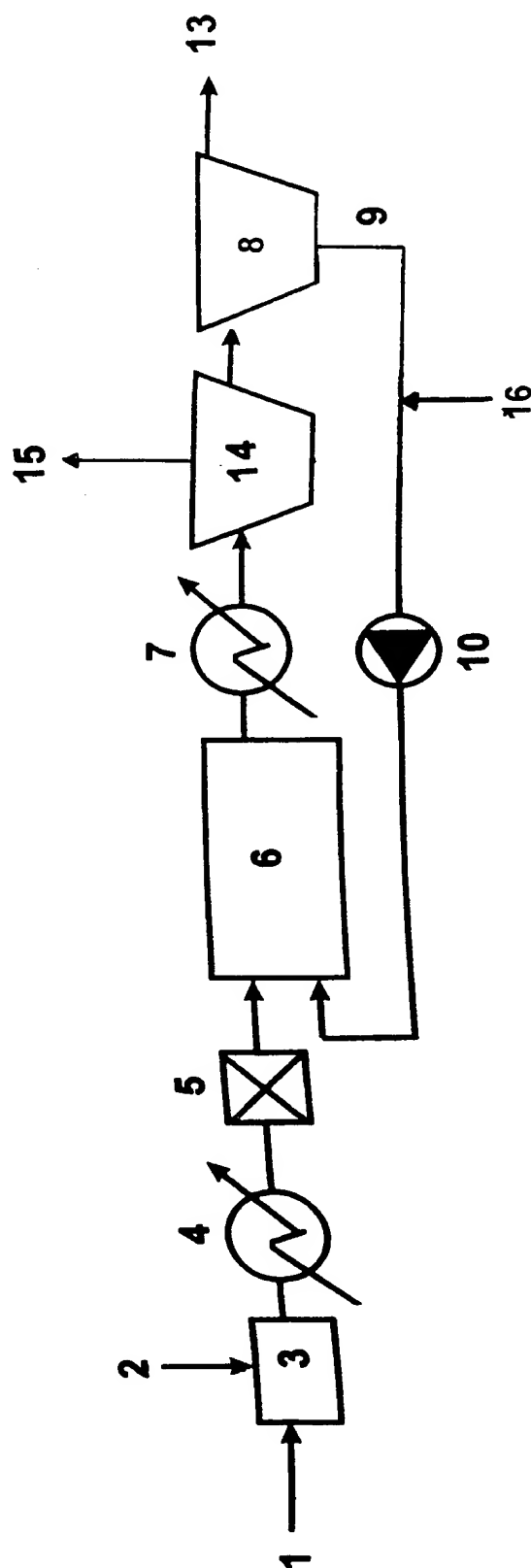


Fig. 2



## INTERNATIONAL SEARCH REPORT

International application No.

PCT/NO 99/00293

## A. CLASSIFICATION OF SUBJECT MATTER

IPC7: F17D 3/14, C10G 33/06

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC7: C10G, F17D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

SE,DK,FI,NO classes as above

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0082630 A1 (IMPERIAL CHEMICAL INDUSTRIES PLC), 29 June 1983 (29.06.83) --	1,12
A	US 5055178 A (SUGIER ET AL), 8 October 1991 (08.10.91) -----	1,12

☐ Further documents are listed in the continuation of Box C.☒ See patent family annex.

\* Special categories of cited documents:

"A" document defining the general state of the art which is not considered to be of particular relevance

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"&amp;" document member of the same patent family

Date of the actual completion of the international search

8 February 2000

Date of mailing of the international search report

16-02-2000

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**INTERNATIONAL SEARCH REPORT**  
Information on patent family members

02/12/99

International application No.  
PCT/NO 99/00293

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